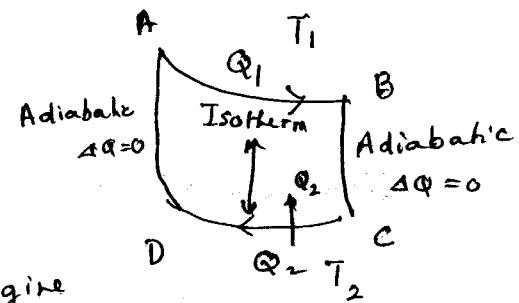


Some revision of essential points with examples

(39)

We will work in the context of Carnot engine

$\Delta W =$ Work done by the system.



(i) The efficiency of the engine

after a cycle is completed is given

$$\Delta Q = \underline{\Delta U + \Delta W} = \Delta W = \cancel{Q_1} - \cancel{Q_2}$$

zero for a cycle

$Q_1 = Q$ into at T_1 the system

$Q_2 = Q$ out of the system at T_2

$$= -Q_{\text{inb. in sys.}} \text{ at } T_2 \\ = Q'_2$$

For ~~reversible engine~~

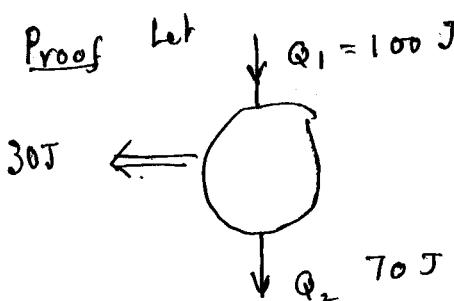
$$\eta = \frac{Q_1 - Q_2}{Q_1} = 1 - \frac{Q_2}{Q_1}$$

For reversible engine

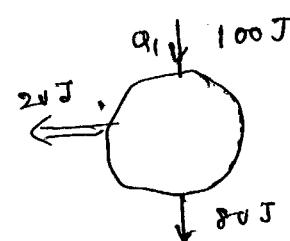
$$\eta = 1 - \frac{Q_2}{Q_1} = 1 - \frac{T_2}{T_1}$$

Any irreversible engine will have an efficiency lower than the reversible Carnot engine. If not it will violate II law in either of the forms.

Proof let



Irreversible

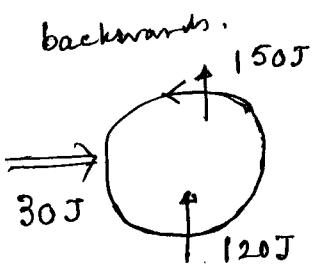


Reversible

Can scale the reversible engine by a factor $\frac{7}{8}$ and run it in the reverse mode. Heat supplied at T_2 is $80 J$ and Heat delivered at $T_1 = 87.5 J$, leaving $12.5 J$ of work on the system. Total Balance : Only $\Delta Q = 12.5 J$ from T_1 converted into $5 J$ Planck violated

We could have scaled it by $\frac{3}{2}$ and sum it
 reversible engine

(40)

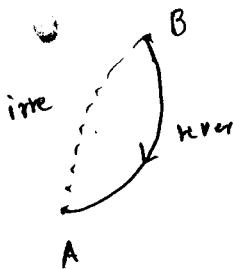


Total is No work done
 50J from T_2 transferred to
 reservoir at T_1 .
 violates clausius.

We also had

$$\frac{Q_1}{T_1} + \frac{Q_2'}{T_2} = 0 \quad \text{for reversible engine and}$$

$$\frac{Q_1}{T_1} + \frac{Q_2'}{T_2} \leq 0 \quad \text{for irreversible engine.}$$



$$\int_A^B \frac{dQ_1}{T} + S(A) - S(B) \leq 0$$

$$\int_A^B \frac{dQ}{T} \leq S(B) - S(A)$$

$$\text{In fine. } \Delta Q \leq T \Delta S.$$

We had introduced three thermodynamic potentials

Enthalpy $H = U + PV$

$$dH = dU + PdV + VdP = \Delta Q + VdP$$

If P is constant

$$dH = d(U + PV) = \Delta Q$$

~~dH~~ If $\Delta Q = 0$ [thermally insulated]

~~$dH = 0$~~ and P is constant.

Example was that Joule-Thomson cooling.

Enthalpy

Consider a reservoir + system

(4)

Closed Fixed entropy and is a maximum.

$U^s + U^r$ must be a minimum. ; No heat exchange
 $\Delta S = 0 \Rightarrow \Delta S^r = 0$

$$d(U^s + U^r) = 0 \quad dU^s + \frac{\partial U^r}{\partial V^r} dV^r = dU^s - p^r dV^r = 0 \\ = dU^s + p^r dV^s = 0$$

$$d(U^s + p^r V^s) = 0$$

$p^s = p^r$ as volume can change (mechanical \equiv^m)

$$d(U^s + p^s V^s) = 0$$

Example is that Joule Thomson effect.

Helmholtz Free energy

$$F = U - TS$$

$$dF = dU - TdS - SdT$$

$$= dU - \Delta Q - SdT$$

$$= -\Delta W_{by} - SdT > dU - TdS - SdT$$

$\Delta W_m > d(U - TS)$ if T is ~~not~~ constant

$$\Delta W_m \gg \Delta F = F_B - F_A$$

if $\Delta F = F_B - F_A > 0$ then more work than ΔF
 is needed to take the system from A to B.

$$\text{if } \Delta F = F_B - F_A < 0 \quad [F_A - F_B > 0]$$

$$F_A - F_B \gg -\Delta W_m = \Delta W_{by}$$

Then the maximum work that can be extracted from the system is $F_A - F_B$

Example 1 Use of Perfect gas.

$$U = \frac{3}{2} NRT \quad S = NR \ln \frac{V}{N} + \frac{3}{2} NR \ln T + \text{Const.}$$

$$F = -NRT \ln \frac{V}{N} + Nf(T) = \left[\frac{3}{2} NRT - NRT \ln \frac{V}{N} + \text{Const} \right]$$

Explained later in detail

Example 2

A solid with sp. ht $C_p = C_v = c$
 Mass 1 kg at temperature T_i
 Touches a reservoir at a lower temperature T_0 .

What is the change in entropy.

$$\underline{\text{Heat Supplied}} \quad c(T_i - T_0)$$

No work extracted.
 Let it be at temp T
 change in entropy.
 and change to $T \pm \Delta T$
 ΔQ given to the reservoir $\left[\Delta Q = c \Delta T \right]$

$$[\text{Entropy decrease}] = c \frac{\Delta T}{T}$$

$$\text{Entropy increase of the reservoir is } \frac{c \Delta T}{T_0}$$

$$\text{decrease for } S(\text{solid}) = c \int_{T_0}^{T_i} \frac{\Delta T}{T} = c \ln \frac{T_i}{T_0}$$

$$\text{Thus } S(\text{solid}) = \frac{c(T_i - T_0)}{T_0}$$

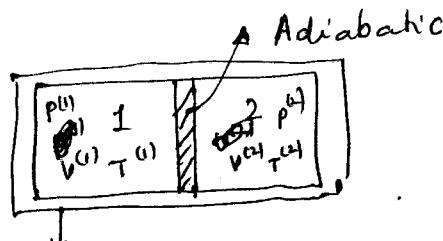
$$\text{Increase for the reservoir} = \frac{c(T_i - T_0)}{T_0}$$

$$\text{Incr} = c \left[\left(\frac{T_i}{T_0} - 1 \right) + \ln \frac{T_i}{T_0} \right] \quad \frac{T_i}{T_0} = x$$

$$= c [x - 1 + \ln x]$$

$$x - 1 + \ln x > 0.$$

Had we changed the temperature of the solid by using a series of reservoirs we could have made the process reversible. [A paper by A. Miranda will be circulated].



one mole on both sides.

Adiabatic

What would be $T_f^{(1)}$, $T_f^{(2)}$ when the wall is allowed to move suddenly.

As there is no contact with outside.

$$S = S^{(1)}(U^{(1)}, V^{(1)}) + S^{(2)}(U^{(2)}, V^{(2)})$$

$$V^{(1)} + V^{(2)} = V = \text{const.}$$

Since each side has $\Delta Q = 0$

$$dU^{(1)} = -p^{(1)}dV^{(1)} \text{ for a small change}$$

$$dU^{(2)} = -p^{(2)}dV^{(2)}$$

Entropy must be maximised.

$$\partial S = \frac{\partial U^{(1)}}{\partial T^{(1)}} + \frac{p^{(1)}dV^{(1)}}{T^{(1)}} + \frac{\partial U^{(2)}}{\partial T^{(2)}} + \frac{p^{(2)}dV^{(2)}}{T^{(2)}}$$

$$= 0 \quad \text{for any situation!}$$

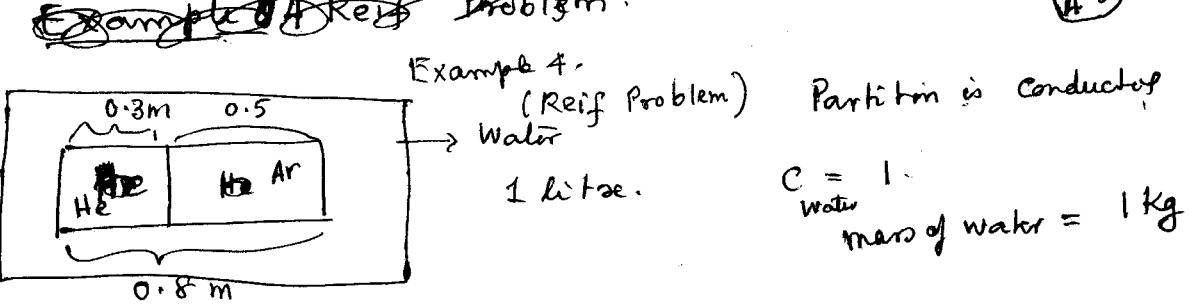
All one can get is

$$V^{(1)} + V^{(2)} = 0, \quad dV^{(1)} = -dV^{(2)}$$

$$\begin{aligned} \partial U^{(1)} &= -\partial U^{(2)} \\ \frac{\partial U^{(1)}}{\partial V^{(1)}} dV^{(1)} &= -\frac{\partial U^{(2)}}{\partial V^{(2)}} dV^{(2)} = \frac{\partial U^{(2)}}{\partial V^{(2)}} dV^{(1)} \end{aligned}$$

$$\text{or } -p^{(1)} = -p^{(2)} \text{ at equilibrium.}$$

Need some more (more) modeling to obtain $T_f^{(1)}$, $T_f^{(2)}$.



He and Ar are 1 mole. Ar at 5 atm, He at 1 atm. The entire system at temp $T = 298^\circ K$. Both are perfect gases.

The partition allowed to move.

- (1) What is the change in temperature of Water
- (2) How far left has the piston come to rest
- (3) What is the increase in entropy of the system.

(1) Let the final temperature be T_f

$$\Delta U_{He} = \frac{3}{2} R (T_f - 298)$$

$$\frac{P_{Ar} V_{Ar}}{298} = n_{Ar} R ; \quad \frac{P_{He} V_{He}}{298} = R$$

$$\frac{P_{Ar}}{P_{He}} \cdot \left[\frac{5}{3} \right] = n_{Ar} \quad \text{PA} \quad n_{Ar} = \frac{1}{3}$$

$$\Delta U_{Ar} = \frac{1}{3} R (T_f - 298)$$

$$= C_V \times 1 (T_f - 298)$$

$$\Delta U_{Water}$$

No exchange with surroundings.

$$\left(\frac{3}{2} R + \frac{R}{3} + C_V \right) (T_f - 298) = 0 \quad \frac{T_f = 298}{\text{No change in temperature!}}$$

(2) Let the final position be V_f , P_f , $T_f = 298^\circ K$.

$$P_f V^{\text{He}} = R \times 298 ; \quad P_f V^{\text{Ar}} = \frac{1}{3} R \times 298$$

$$\frac{V^{\text{He}}}{V^{\text{Ar}}} = \frac{1}{3} \quad \frac{V^{\text{He}} + V^{\text{Ar}}}{V^{\text{Ar}} \left(1 + \frac{1}{3} \right)} = 0.8 \quad \frac{V^{\text{Ar}}}{4} = 0.6$$

$$V^{Ar} = \frac{V^{He}}{3} \quad V^{Ar} + V^{He} = 0.8 m \times S$$

$$\left(\frac{1}{3} + 1\right) V^{He} = 0.8 \times S$$

$$V^{He} = 0.6 \times S$$

S = Area of cross section of the container.

$$S_f - S_i = R \ln \left[\frac{0.6}{0.3} \right] + \frac{R}{3} \ln \left[\frac{0.2}{0.15} \right]$$

+ 0 (for water - as it has not been heated)

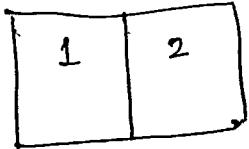
(used $S = \frac{N}{2} R \ln T + N R \ln v$)

$S_f - S_i = R \times 0.38 = 3.2 \text{ J/K}$

[Convert Atmospheres to Pascals].

Comments on Example 3 From A-E. Curzon ATP 37, 404 (1969)

Consider an isolated box containing gas in the two chambers 1 and 2, separated by a partition.



No exchange of matter.

We have

$$dU_1 + dU_2 = 0 \quad (1)$$

$$dV_1 + dV_2 = 0, \quad (2)$$

$$T_1 dS_1 = dU_1 + p_1 dV_1 \quad (3)$$

$$T_2 dS_2 = dU_2 + p_2 dV_2 \quad (4)$$

Let the partition move : Equilibrium when $S_1 + S_2$ is a maximum

$$d(S_1 + S_2) = 0$$

(a) Perfect conductor.

$$dS = \left[\frac{dU_1}{T_1} + \frac{p_1}{T_1} dV_1 \right] + \left[\frac{dU_2}{T_2} + \frac{p_2}{T_2} dV_2 \right]$$

$$(dU_1 = -dU_2) \& (dV_1 = -dV_2)$$

$$dS = \left[dU_1 \left(\frac{1}{T_1} - \frac{1}{T_2} \right) + \left[\frac{p_1}{T_1} - \frac{p_2}{T_2} \right] dV_1 \right]$$

dU_1 and dV_1 are independent Thus $T_1 = T_2$ & $p_1 = p_2$.

(b) Perfect insulator. dU_1 and dV_1 are not independent.

$$\begin{array}{ll} 1 & \Delta Q_1 = 0 \text{ and } dS_1 \geq 0 \\ 2 & \Delta Q_2 = 0 \text{ and } dS_2 \geq 0 \end{array}$$

Given $dS_1 + dS_2 = 0$ [for $\Sigma S_1 + S_2$ must be maximum]

$$dS_1 = dS_2 = 0$$

$$dU_1 = -P_1 dV_1, \quad dU_2 = -P_2 dV_2$$

~~$$dS = \left(\frac{1}{T_1} + \frac{1}{T_2} \right) P_1 dV +$$~~

$$dS_1 = \frac{dU_1}{T_1} + \frac{P_1 dV_1}{T_1}, \quad dS_2 = \frac{dU_2}{T_2} + \frac{P_2 dV_2}{T_2}$$

$$dS = \left[\left(\frac{1}{T_1} - \frac{1}{T_2} \right) (-P_1 dV_1) + \left(\frac{P_1}{T_1} - \frac{P_2}{T_2} \right) dV_2 \right]$$

from (A)

$$\therefore \left(\frac{P_1}{T_2} - \frac{P_2}{T_2} \right) dV_1 = 0$$

$$\therefore P_1 = P_2$$

No conclusion about T_1 & T_2